



2020 AFPM SUMMIT

Excellence in Plant Performance

AFPM WEBINAR
SERIES:

REBOILER

CIRCUITS FOR

TRAYED COLUMNS

APRIL 30, 2020

WHAT IS AFPM WEBINAR SERIES?

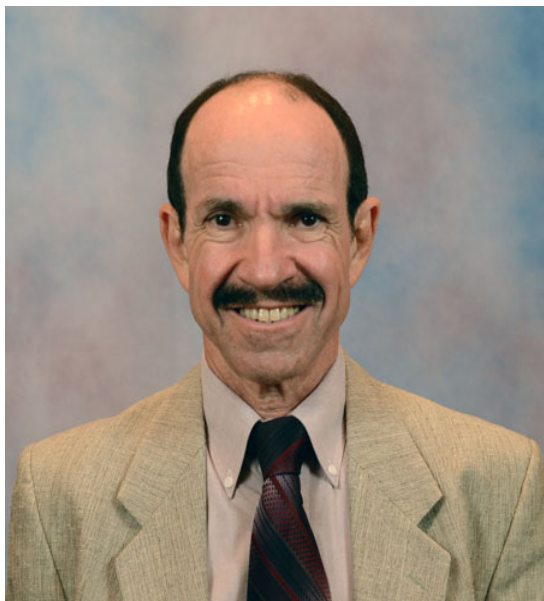
- As we embark in developing The Summit, Excellence in Plant Performance, there will be more opportunity for member engagement
- There will be one webinar a month until the August Summit :
 - May 20 - 21, 2020 - “Learning Teams” - A Two Part Series**
 - Michael Vopatek, Maintenance Manager, LyondellBasell
 - Sahika Korkmaz, Senior Human Performance Advisor, Chevron
 - Chelsea Miller, Human Performance Advisor, Chevron
 - June - Gasoline Processing**
 - July - Operational Planning, Control & Automation Technologies**

GIVE US YOUR FEEDBACK!

- Please fill out this quick survey:

<https://www.surveymonkey.com/r/XTNB3SB>

PRESENTER



Henry Kister
Senior Fellow
Director of Fractionation
Technology
Fluor

- 30 years experience in design, troubleshooting, revamping, field consulting, control and startup of fractionation processes and equipment
- Author of 3 books, distillation equipment chapter of Perry's Handbook, distillation chapter in the Kirk-Othmer Encyclopedia of Chemical Technology, over 120 articles
- Taught the IChemE-sponsored "Practical Distillation Technology" course over 530 times in 26 countries
- Recipient of several engineering awards
- BE and ME from the University of New South Wales in Australia
- Fellow of AIChE, IChemE, member of the US National Academy of Engineering
- Serves on the FRI Technical Advisory and Design Practices Committees

Reboiler Circuits

Part 1: Reboiler Selection

Fractionation Research Inc.
Design Practices Committee

AFPM Webinar April 30, 2020
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Members of the Fractionation Research Inc. Design Practices Committee

Ray Sowiak, Chairman, Mc Dermott Technology

Joe Parker, Vice Chairman, Eastman Chemical Company

Brendan Ackers, E.I. Dupont De Nemours & Company

Jeremy Brauer, UOP LLC

Bradley Haecker, The Dow Chemical Company

Henry Z. Kister, Fluor Corporation

Paul Morehead, P.E. Koch-Glitsch, LP

Bill Nelson, CITGO

Ron Olsson, P.E. Celanese Ltd

John Petrik, Air Products and Chemicals

Attilio Praderio, ConocoPhillips Company

Dan Summers, P.E. Sulzer Chemtech USA Inc.

Dr. Zhongcheng Wang, ExxonMobil Research and Engineering Company

Keith Whitt, Shell Global Solutions

Dr. Simon Xu, Technip FMC

Dr. Norman Yeh, ExxonMobil Upstream Integrated Solutions

Tim Zygula, BASF Petrochemicals

Lowell Pless, Consultant, Tracerco (Retired)

John P. Farone, Consultant, Dow Chemical (Retired)

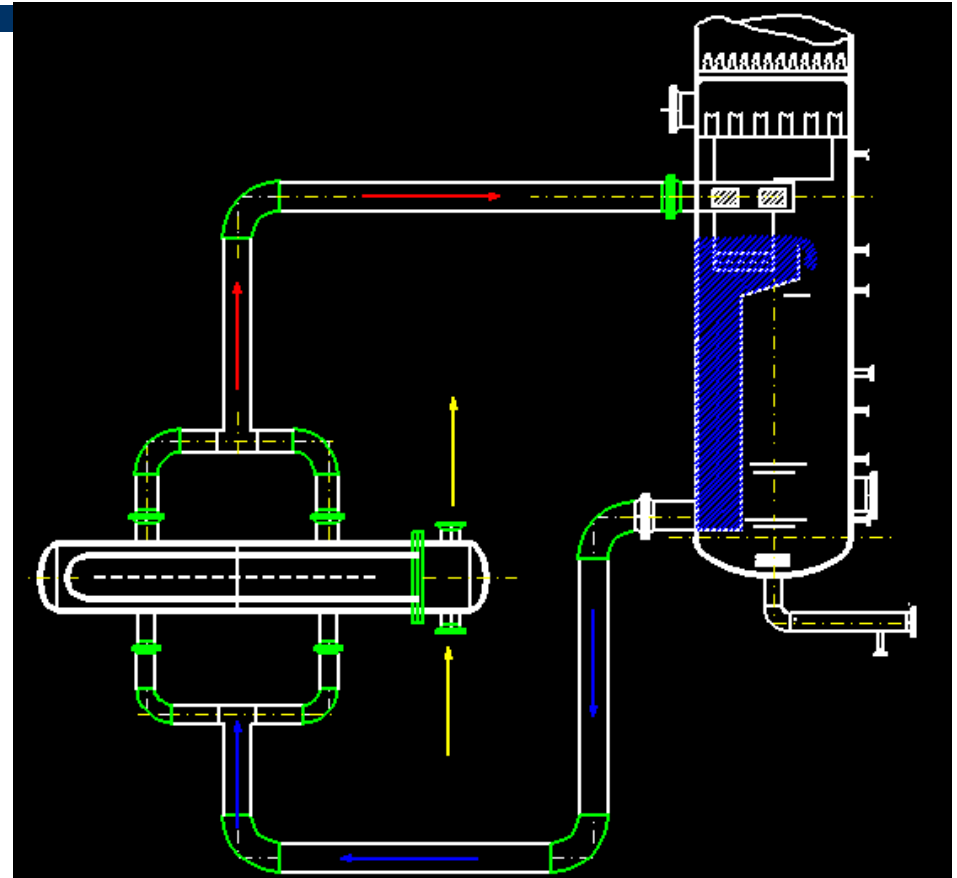
Reboiler Circuits

Disclaimer

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Introduction

- ▶ Tower bottoms and reboiler circuits should be considered as key tower internals
- ▶ Overall tower performance is dependent on a proper design of both tower bottoms and reboiler
- ▶ Taken together they are thought to be the second-most common cause of tower problems



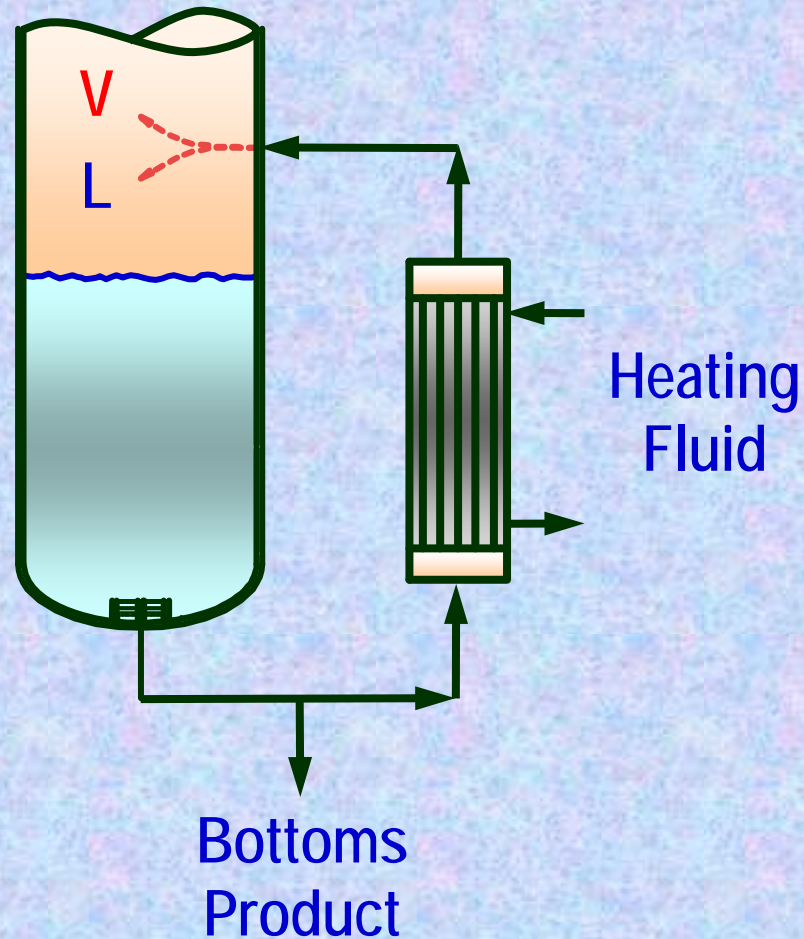
Example of a complex geometry:
Recirculating horizontal
Thermosiphon with constant head
internal baffle.

Reboiler Selection Considerations

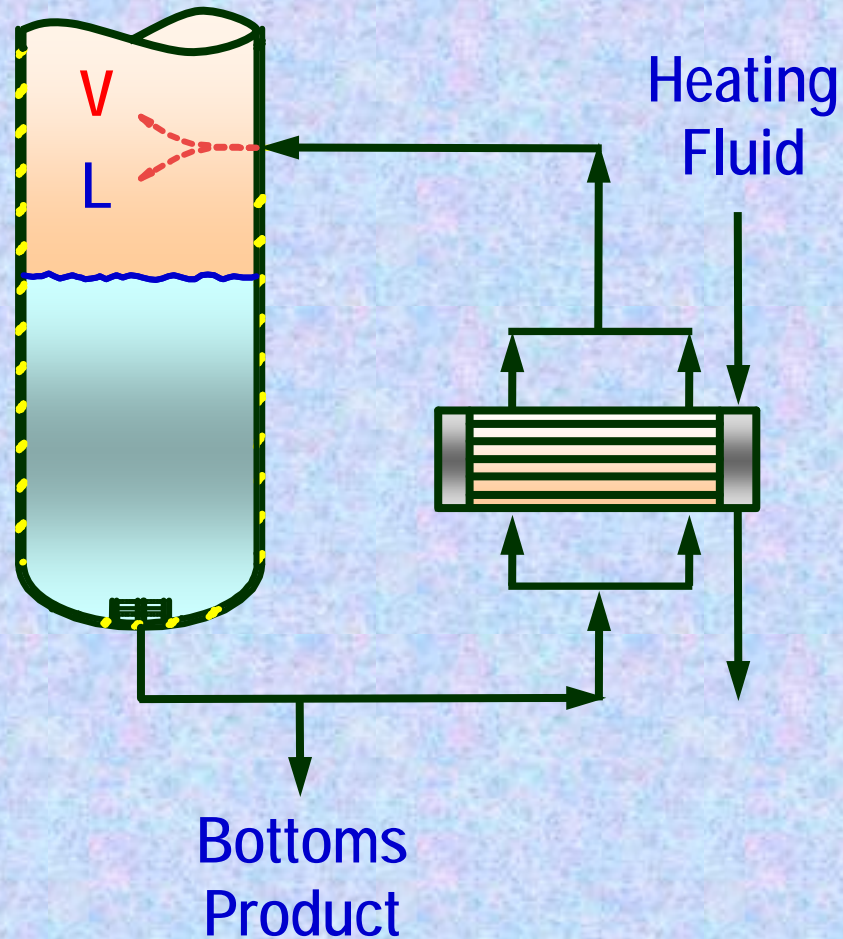
- ▶ Thermosiphons should be considered first
 - Gravity flow systems – utilize the density difference between the feeding liquid and mixed phase fluid in the return
 - Tend to be the most economical
 - Compact – smaller heat exchangers
 - Minimum plot space for vertical exchangers
 - Require no pumps
 - Low to moderate fouling tendency
 - Low residence times
 - Most widely used type in distillation
- ▶ Not applicable to all systems
 - High liquid viscosity (>10 cP)
 - Heavily fouling systems
 - Adequate driving head not available
 - Large operating load variation
 - When high reliability is critical

Thermosiphons can sometimes be problematic in vacuum where small liquid head variations largely impact the boiling point, leading to large & head-dependent preheat zone in the reboiler. Can be mitigated by a constant head and good design.

Circulating Vertical Thermosiphon



Circulating Horizontal Thermosiphon



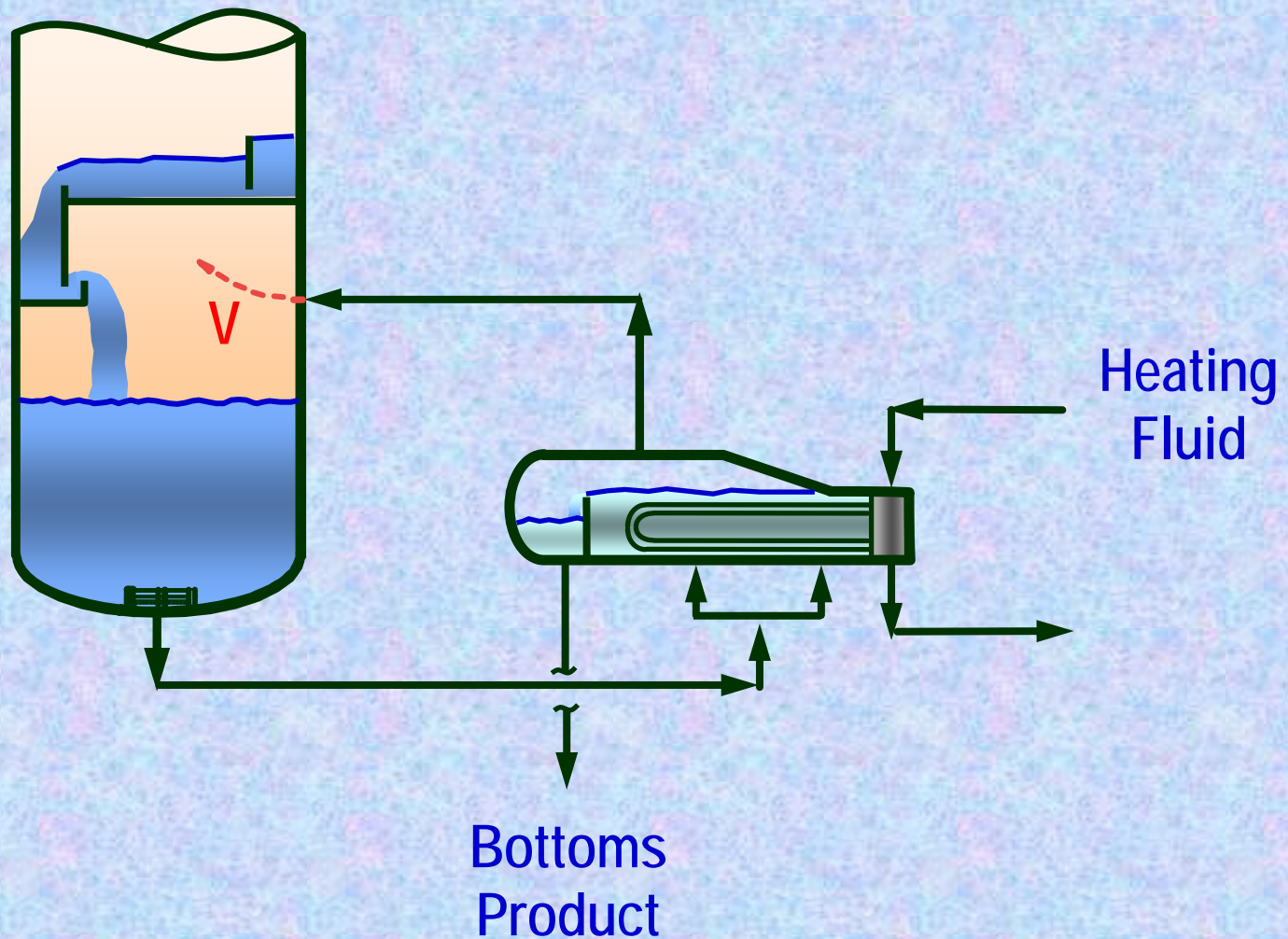
Vertical or Horizontal ?

- ▶ Literature gives confusing accounts
 - Vertical exchangers predominate in chemical industry
 - Limited in tube length
 - Horizontal are more common in refining applications

- ▶ Vertical Preferred
 - Minimum plot space
 - Minimum return piping
 - Fouling process side
 - High pressure process side
 - Less expensive

- ▶ Horizontal Preferred
 - Large heat transfer area
 - Minimize skirt height
 - Fouling heating side
 - High pressure heating medium
 - Better access for maintenance

Standard Kettle



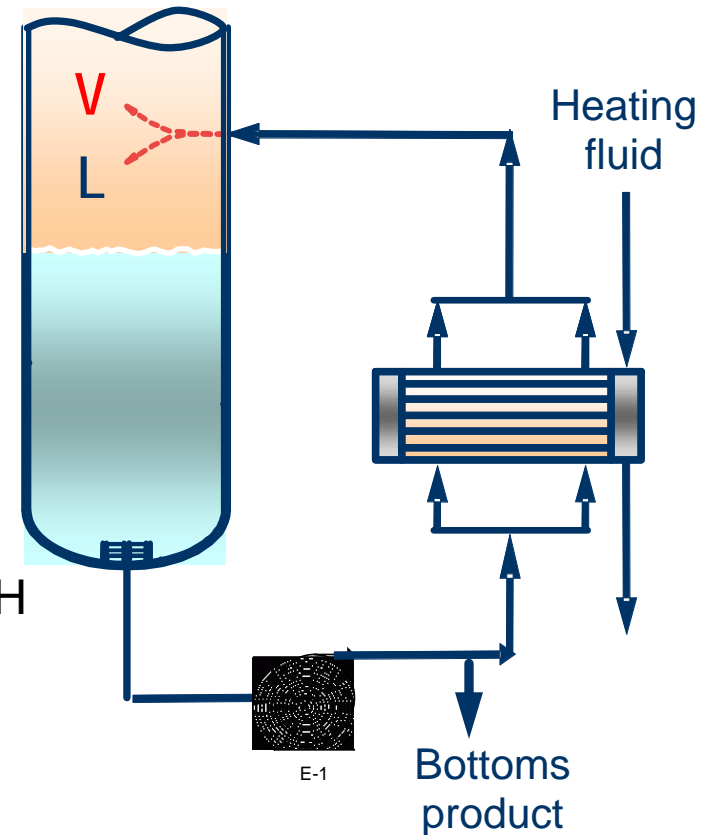
Kettle?

- ▶ Kettles are the next most widely used reboiler types
 - Reliability – composition instability & large flow operating load variation
 - Small driving head requirements (smaller skirt height)
 - Ability to handle large surface areas in a single shell
- ▶ Kettles have the following disadvantages:
 - High capital cost – low heat transfer rate
 - Not recommended for process fouling services
 - Not recommended for high viscosity liquids
 - High residence time

Forced Circulation?

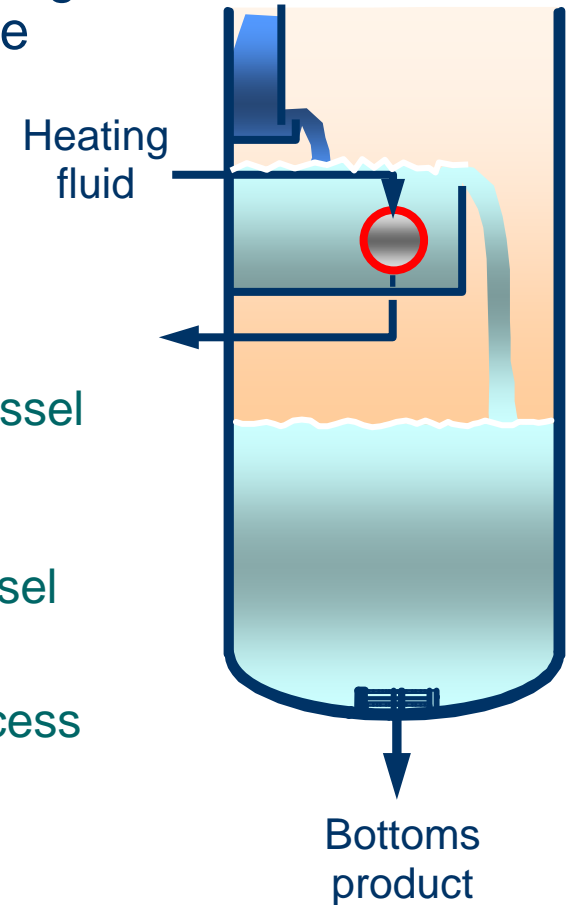
- ▶ Forced circulation – the reboiler feed liquid is pumped through either the tube side of a vertical or shell side of a horizontal exchanger

- High heat transfer rate
- Good for high viscosity liquids
- System of choice for fouling systems
- Good for instability type systems
- Additional operating and capital cost
 - Pump – cost, maintenance, sparing
 - Controls
 - Piping, valves
 - Additional skirt height for pump NPSH
- Safety – potential for leaks and fire



Internal Reboiler?

- ▶ Internal reboiler – exchanger tubes are submerged either in a tub or liquid bottom sump inside the tower
 - Not widely used
 - Clean system
 - Low heat transfer
 - Low surface area
 - Mechanical design of internal supports and vessel flange must be considered
 - Additional tower height
 - Difficult to maintain – access only through vessel
- ▶ Advantages:
 - Low capital cost – no pressure vessel, no process piping
 - No plot space



Reboiler Circuits

Part 2: Tower Bottom

Arrangements

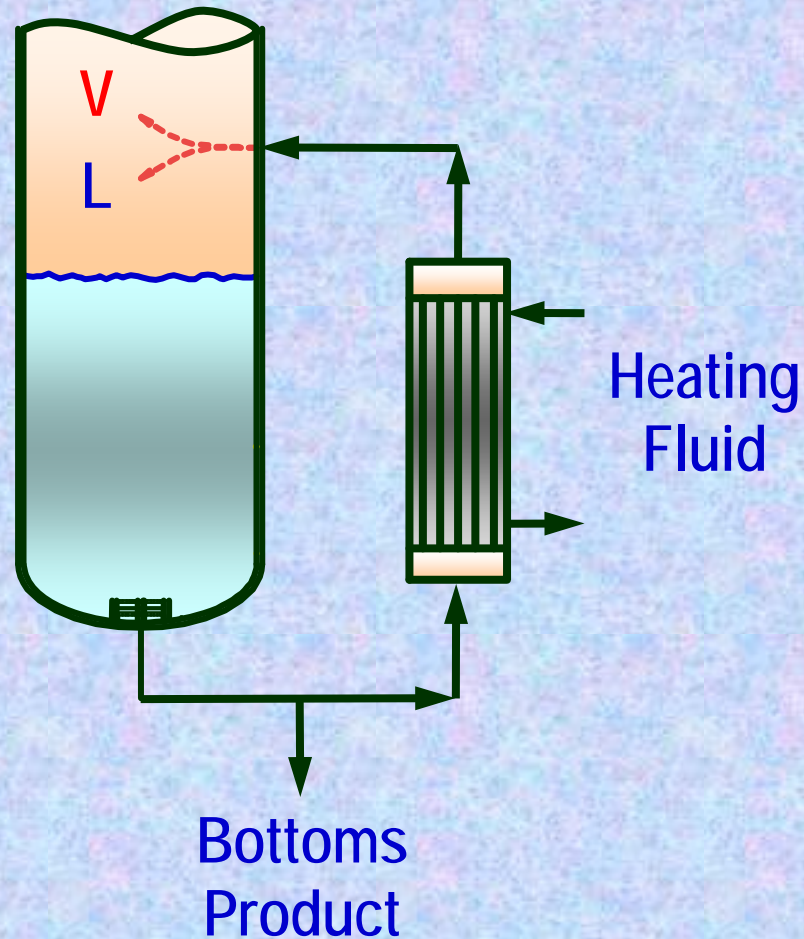
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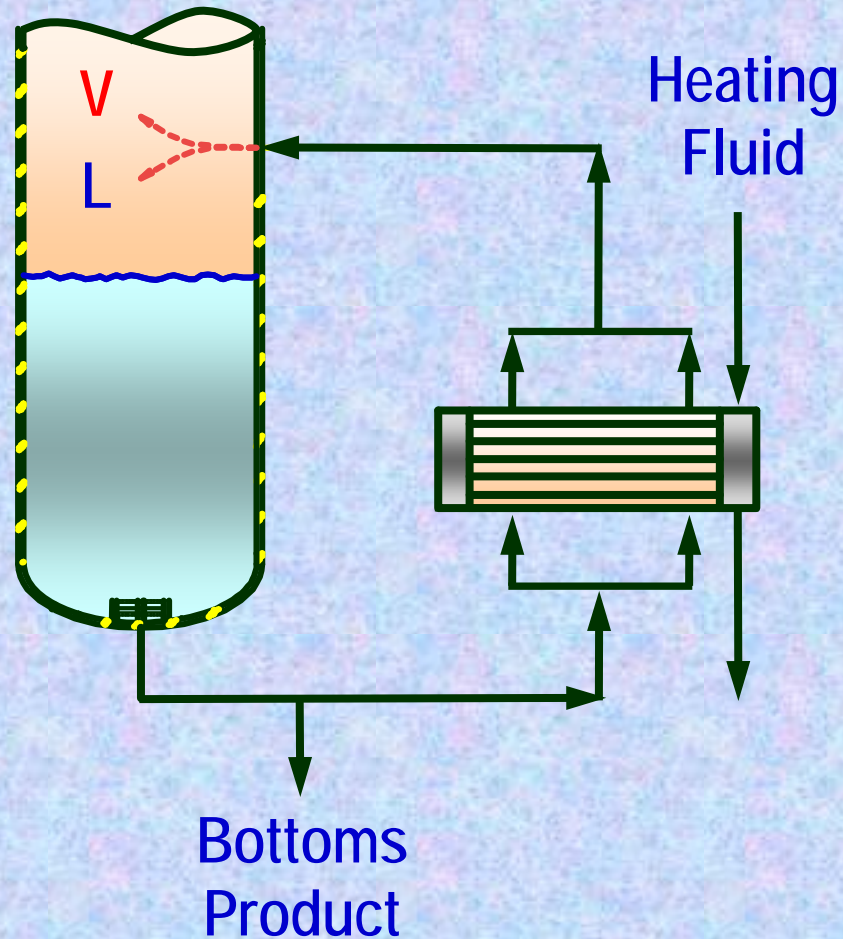
Recirculating Vs. Once-Through

- In once-through, bottom tray liquid traverses through reboiler once
- Recirculating portion of the reboiler effluent mixes with the reboiler feed

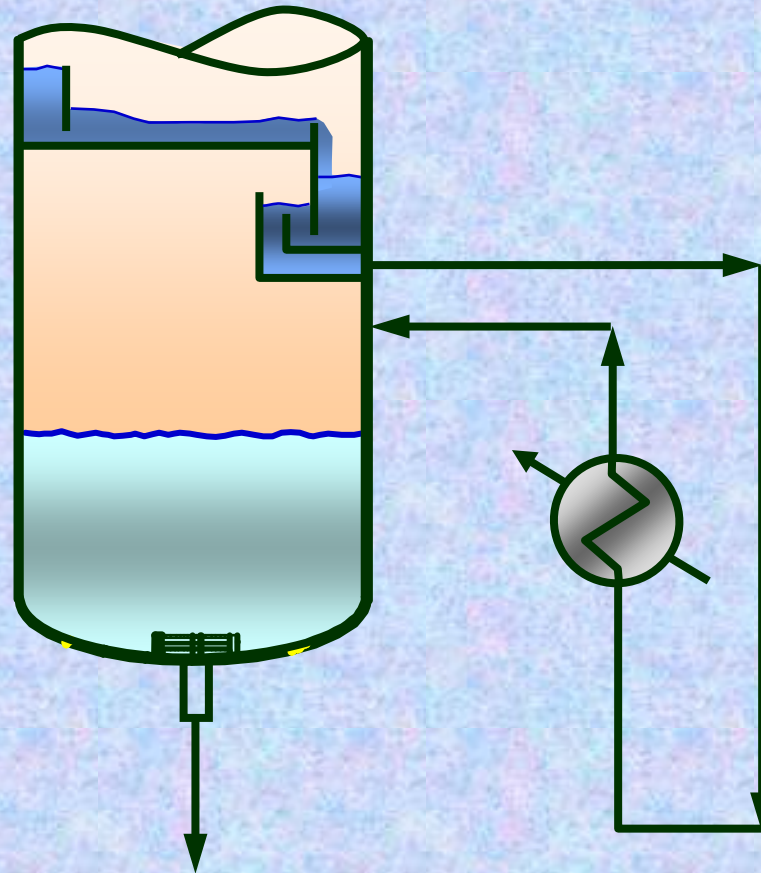
Circulating Vertical Thermosiphon



Circulating Horizontal Thermosiphon

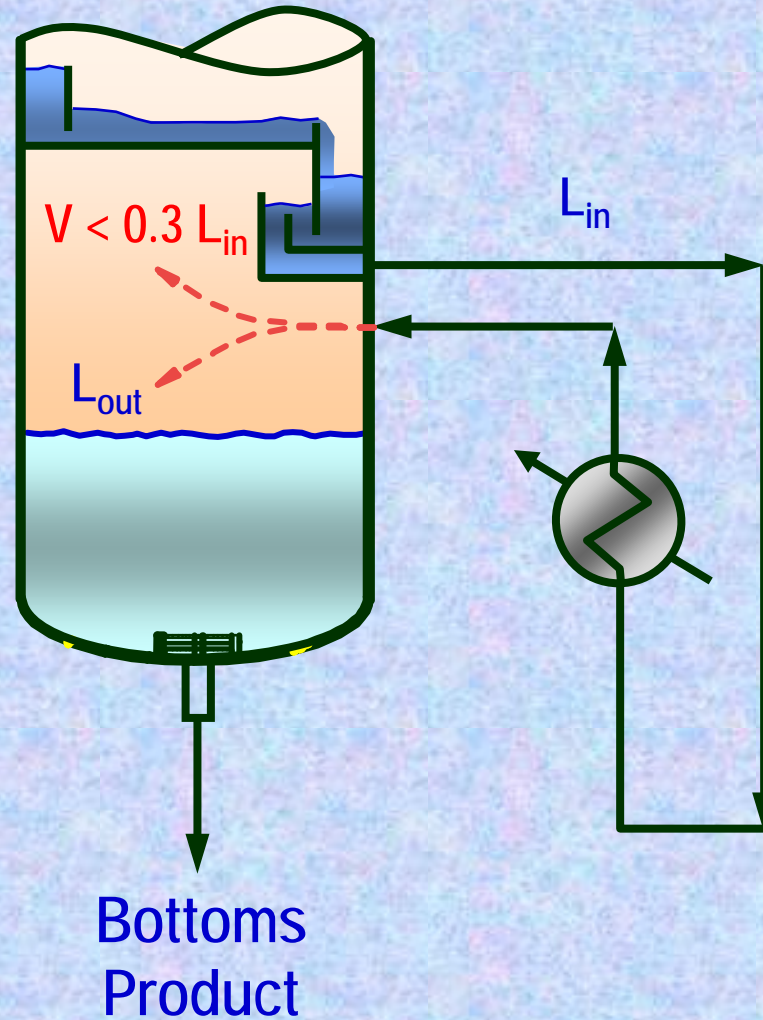


Once Through Thermosiphon Trapout

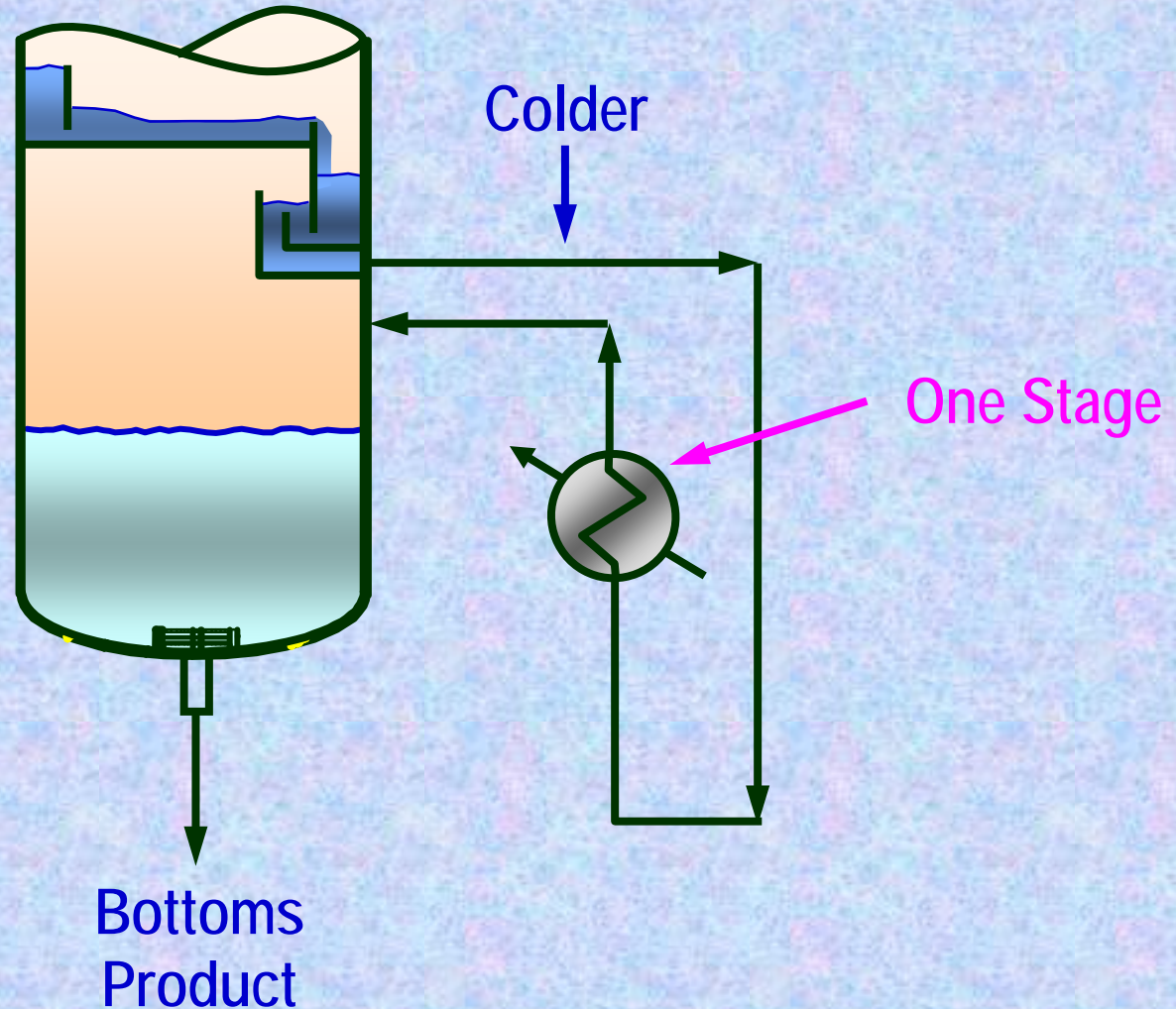


Bottoms Product

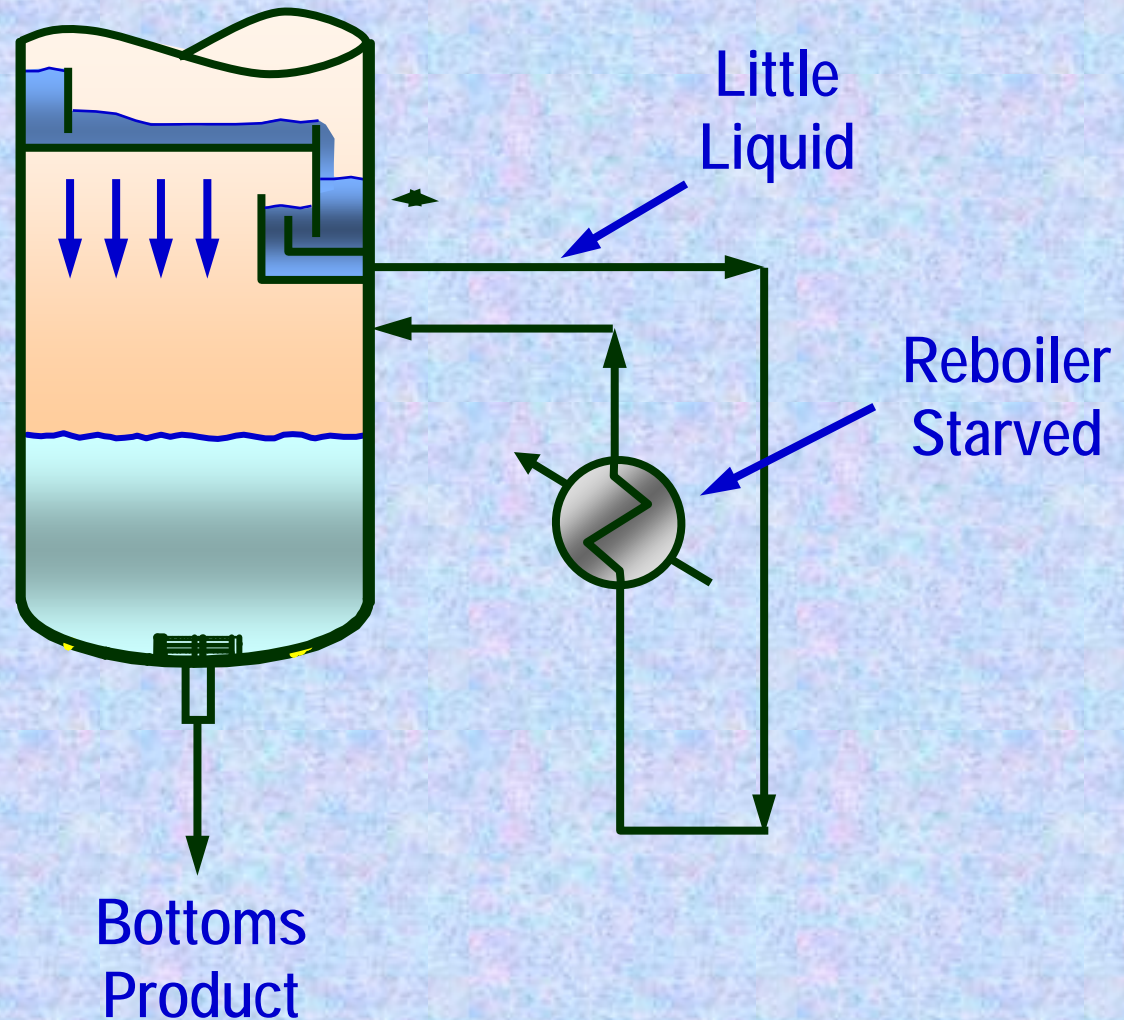
Once Through Thermosiphon Trapout



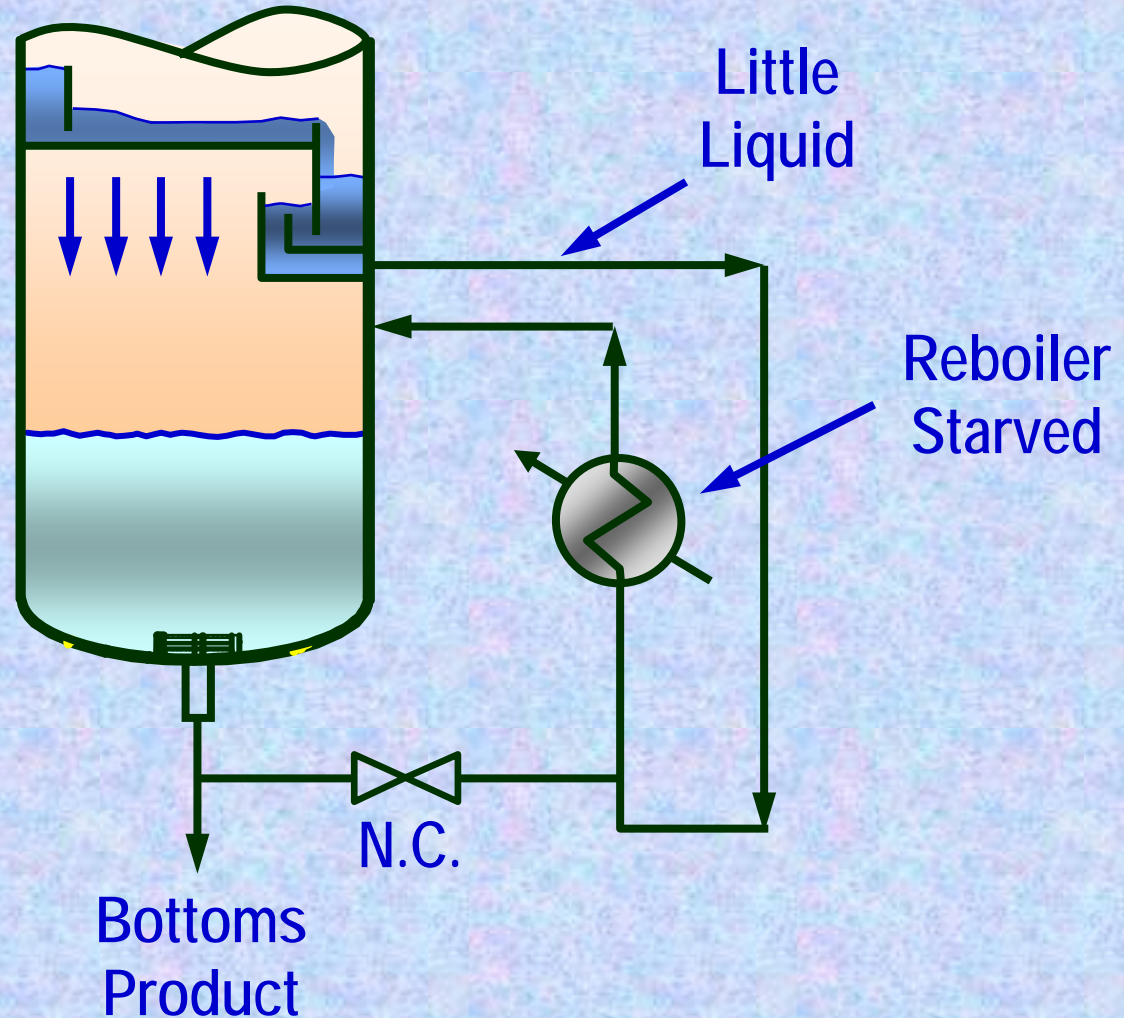
Once Through Thermosiphon Trapout



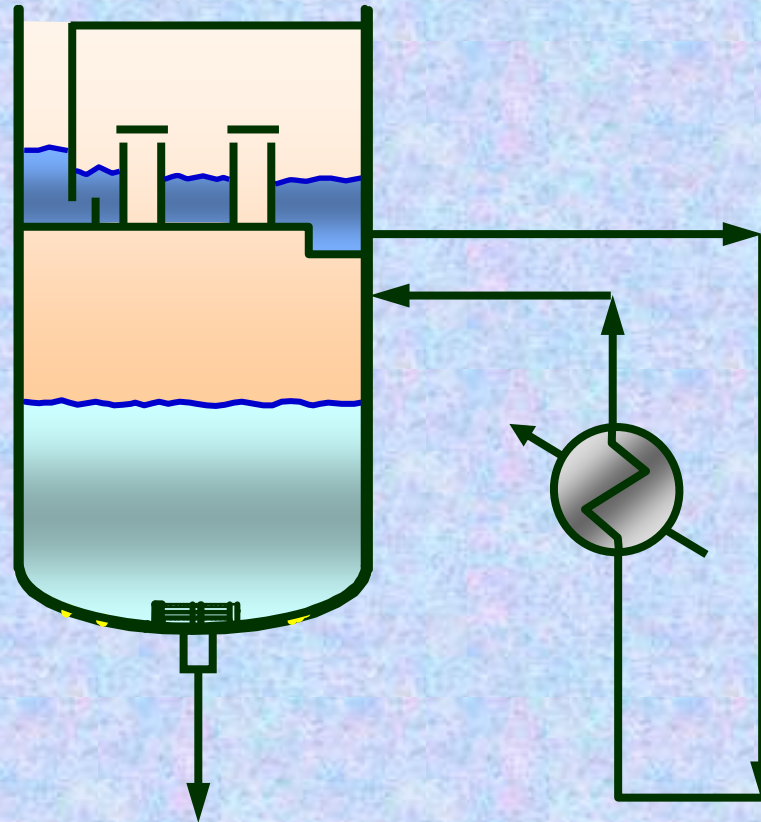
Once Through Thermosiphon Trapout



Once Through Thermosiphon Trapout

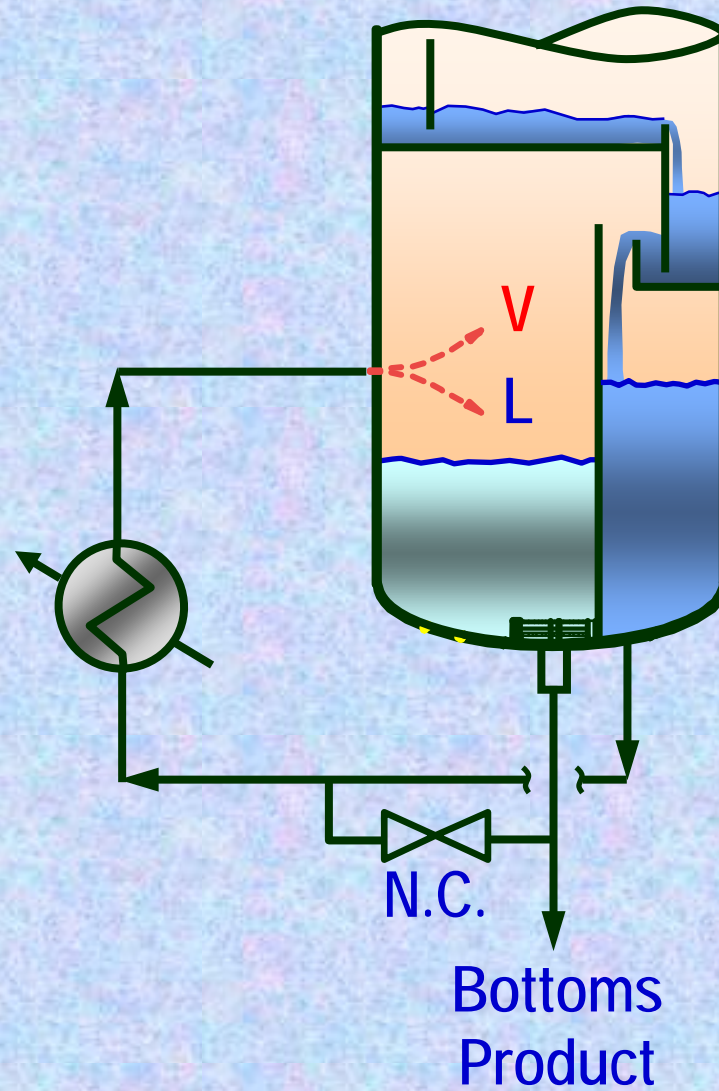


Once Through Thermosiphon Collector Tray

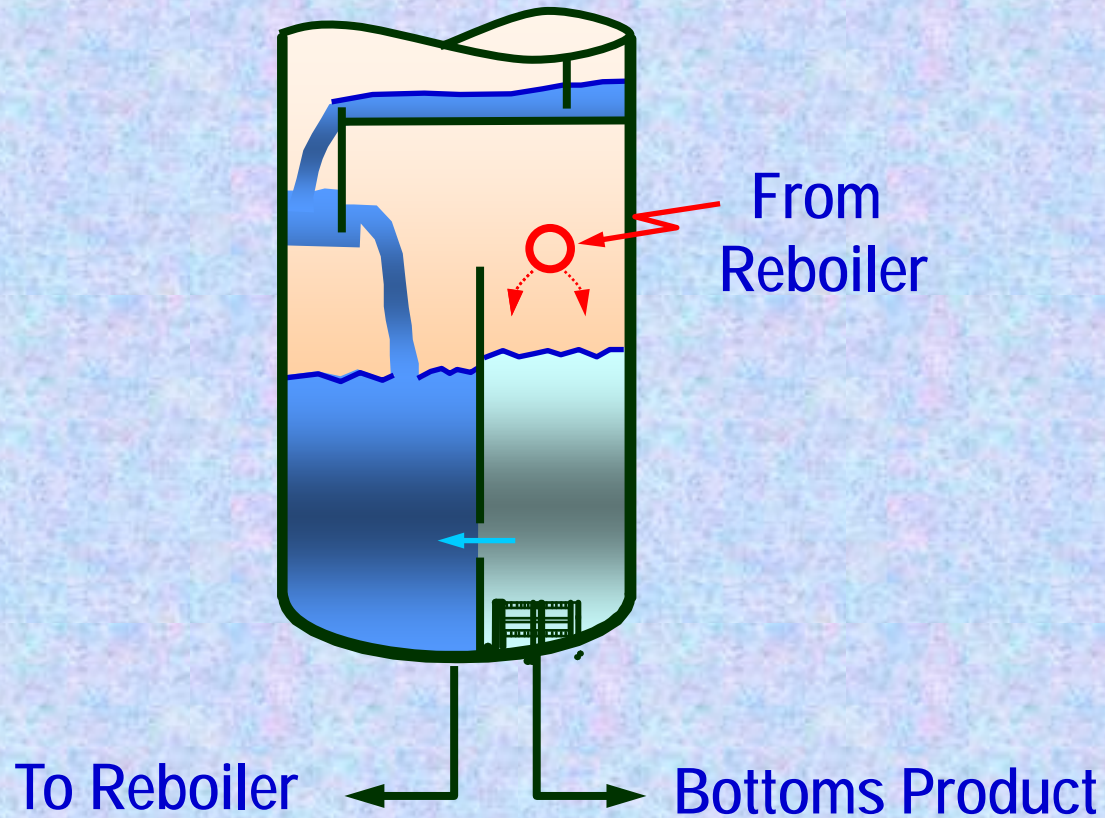


Bottoms
Product

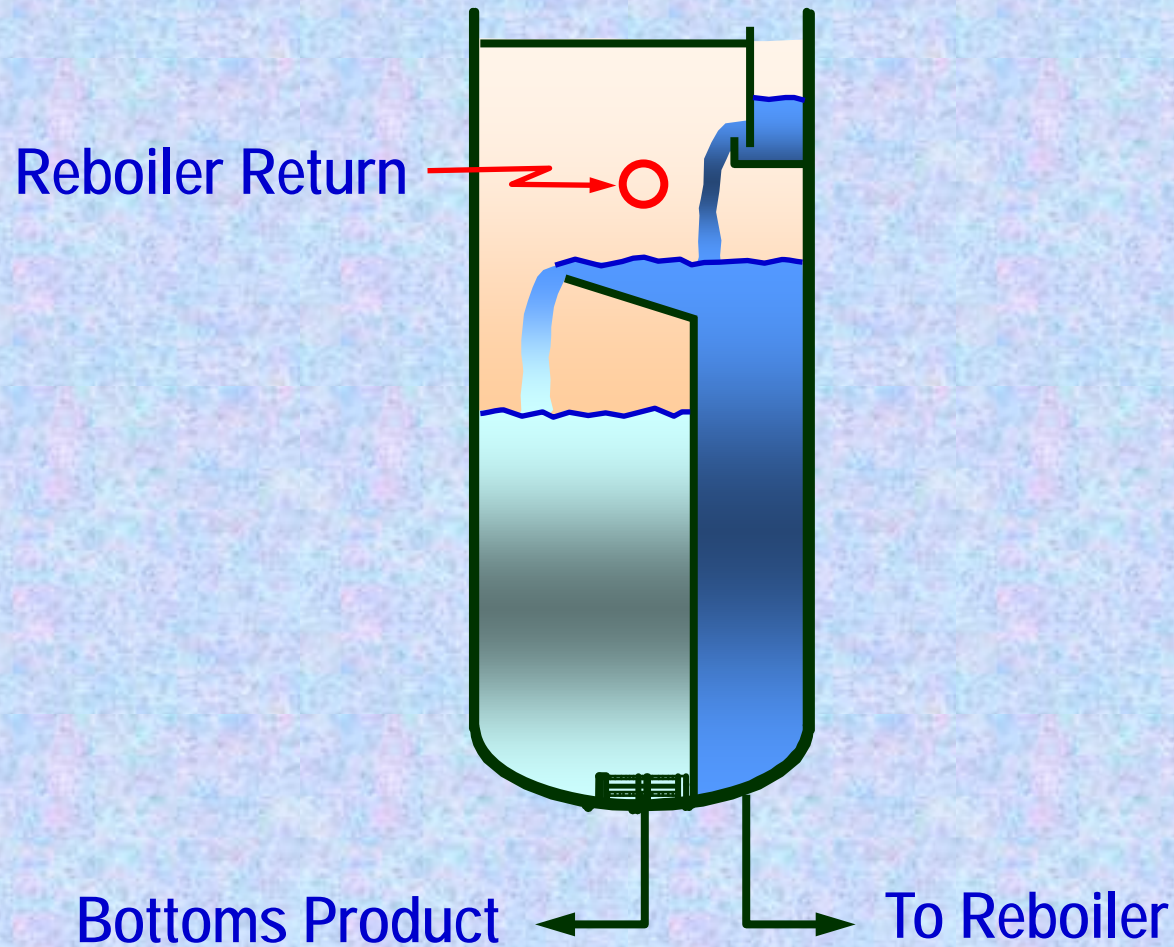
Once Through with Baffle



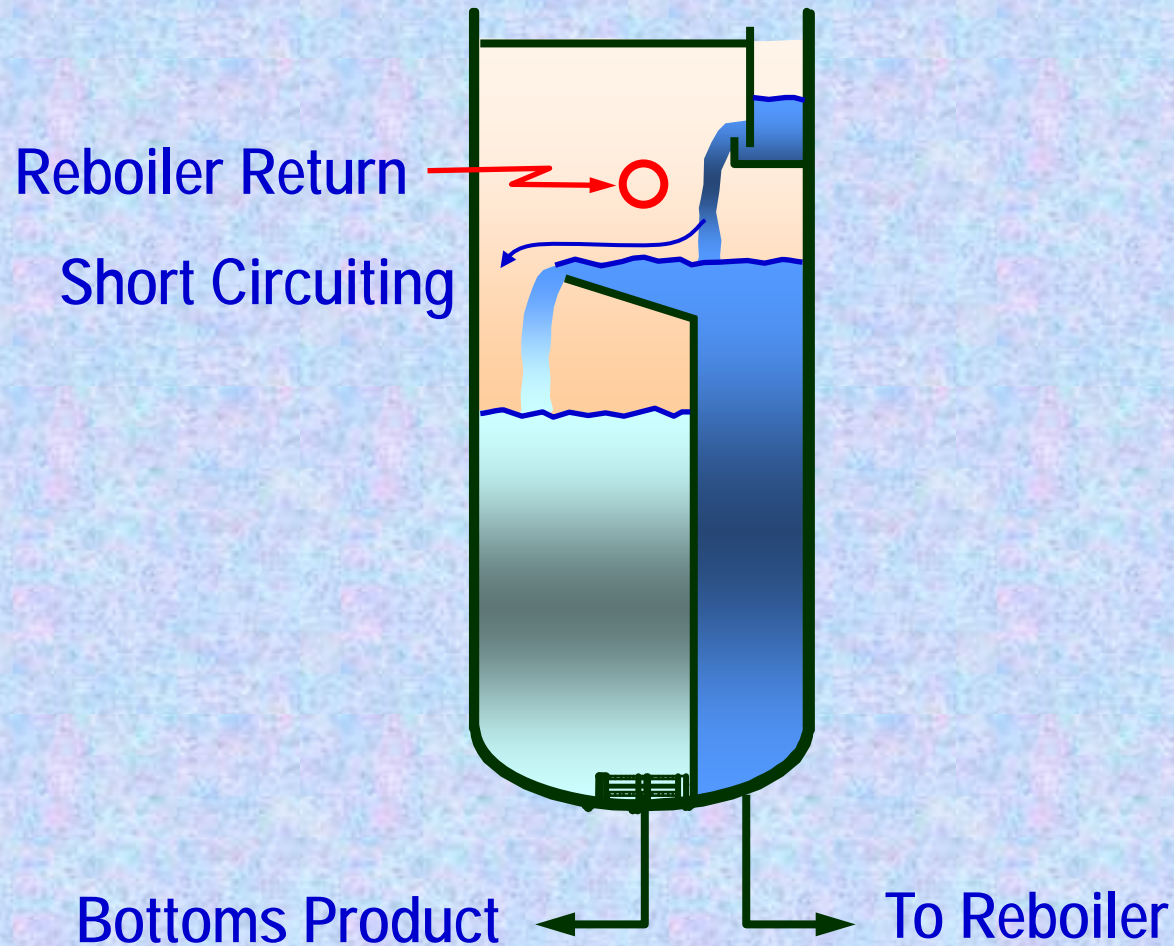
Preferential Baffle



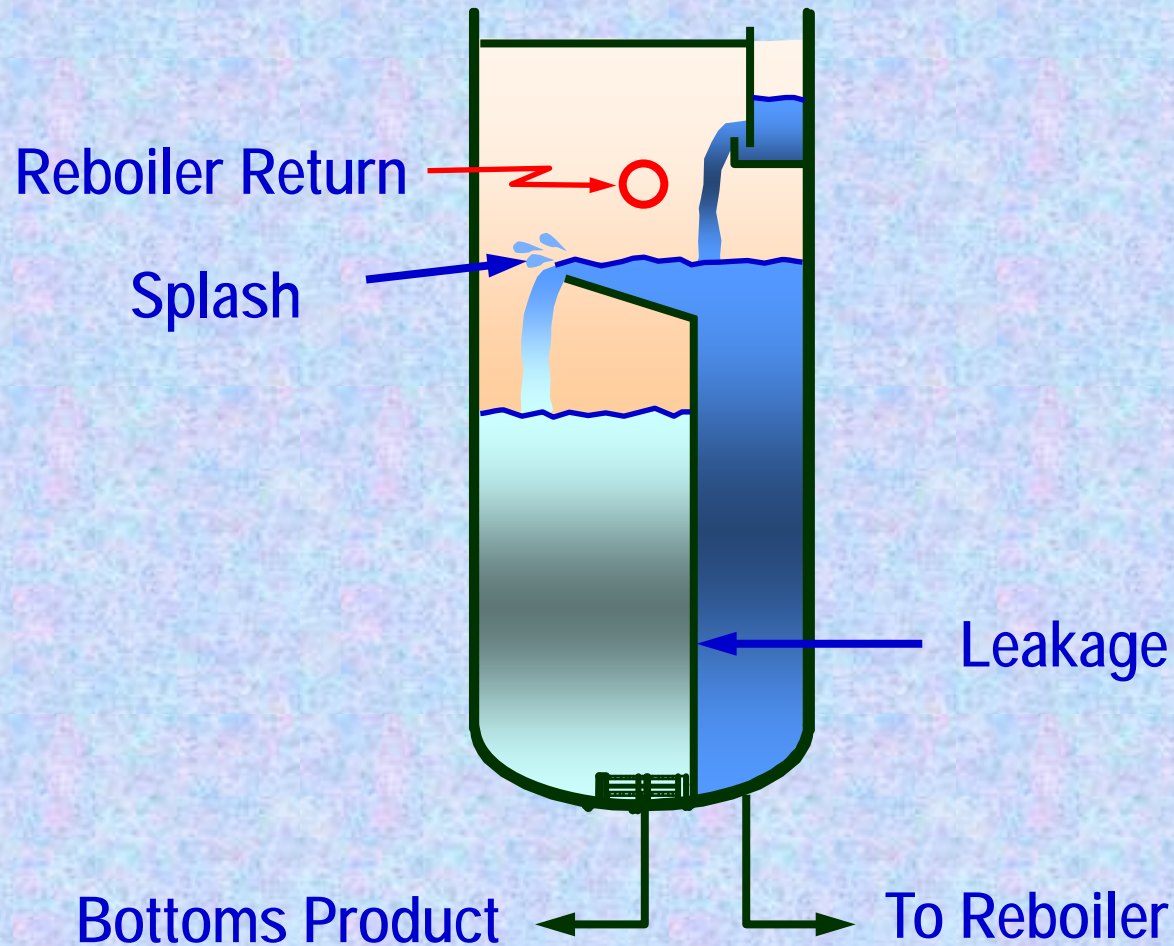
Constant Head with Reboiler Baffle



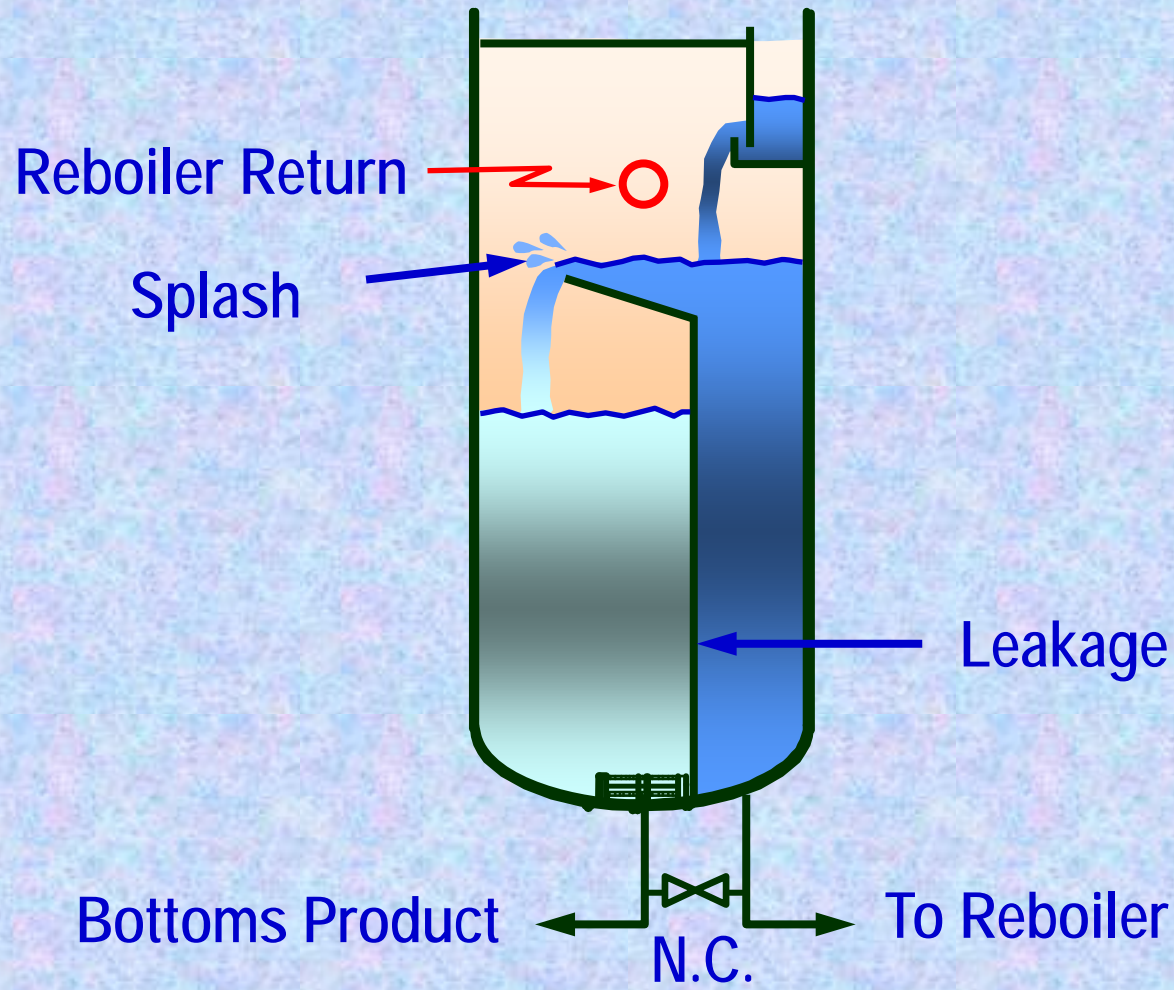
Constant Head with Reboiler Baffle



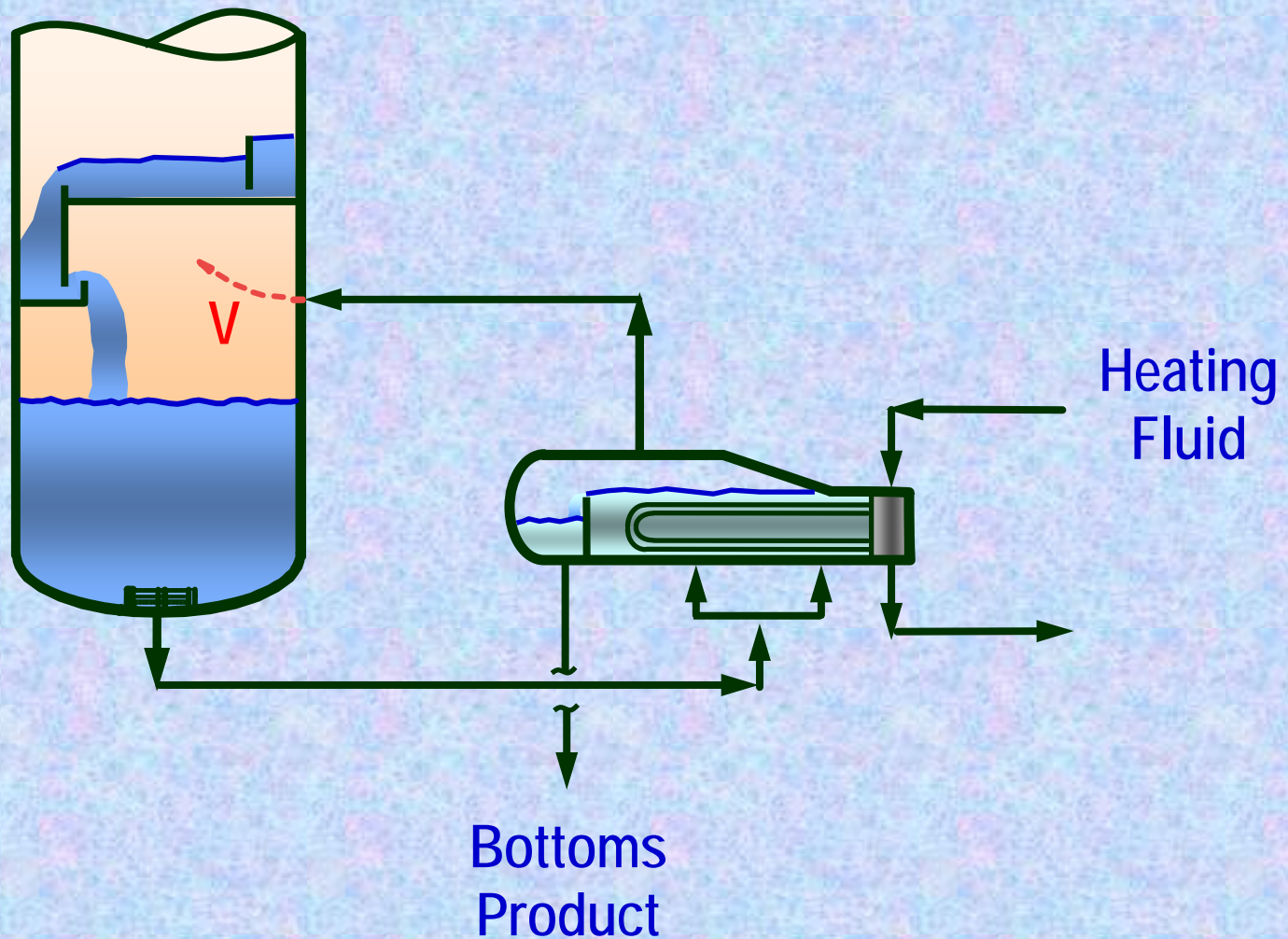
Constant Head with Reboiler Baffle



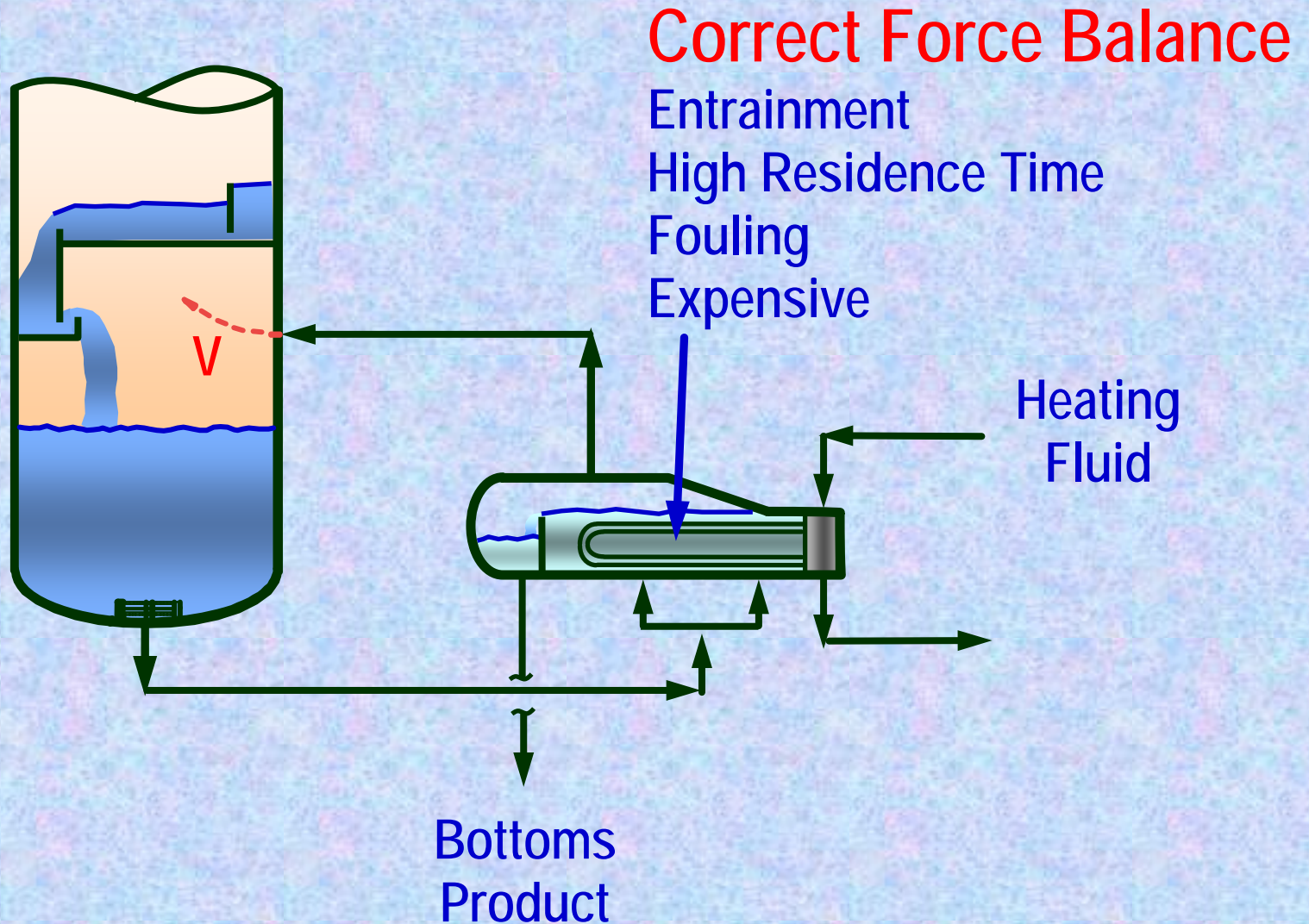
Constant Head with Reboiler Baffle



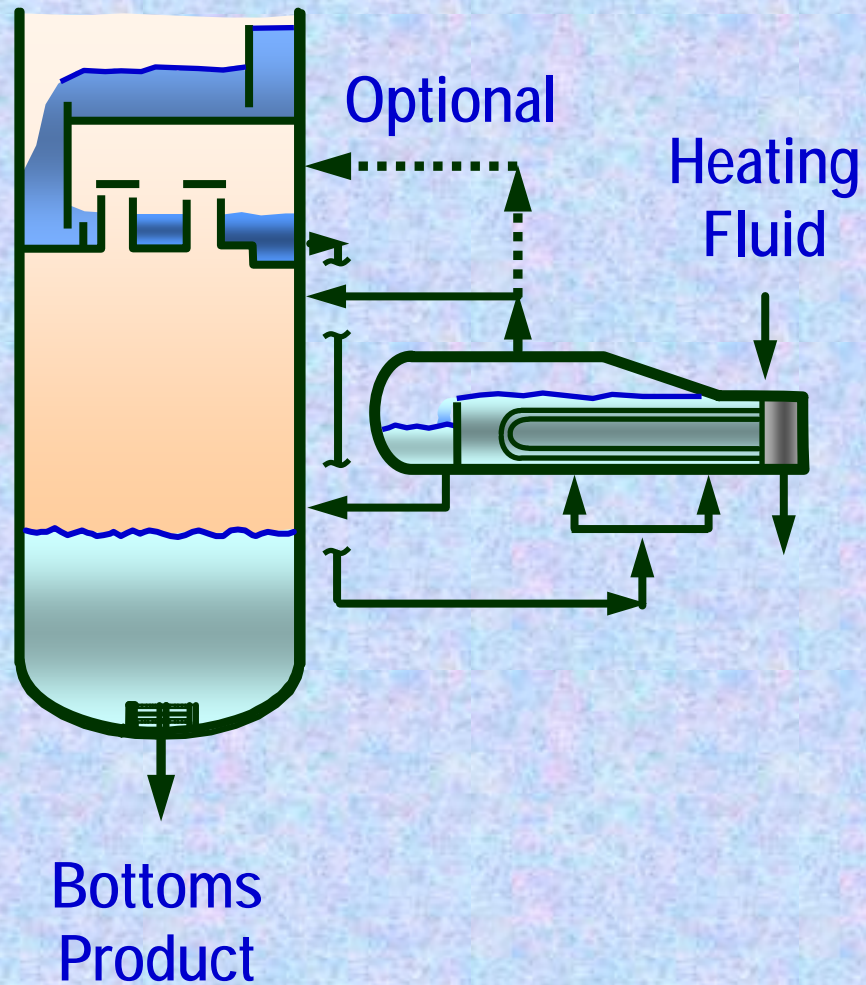
Standard Kettle



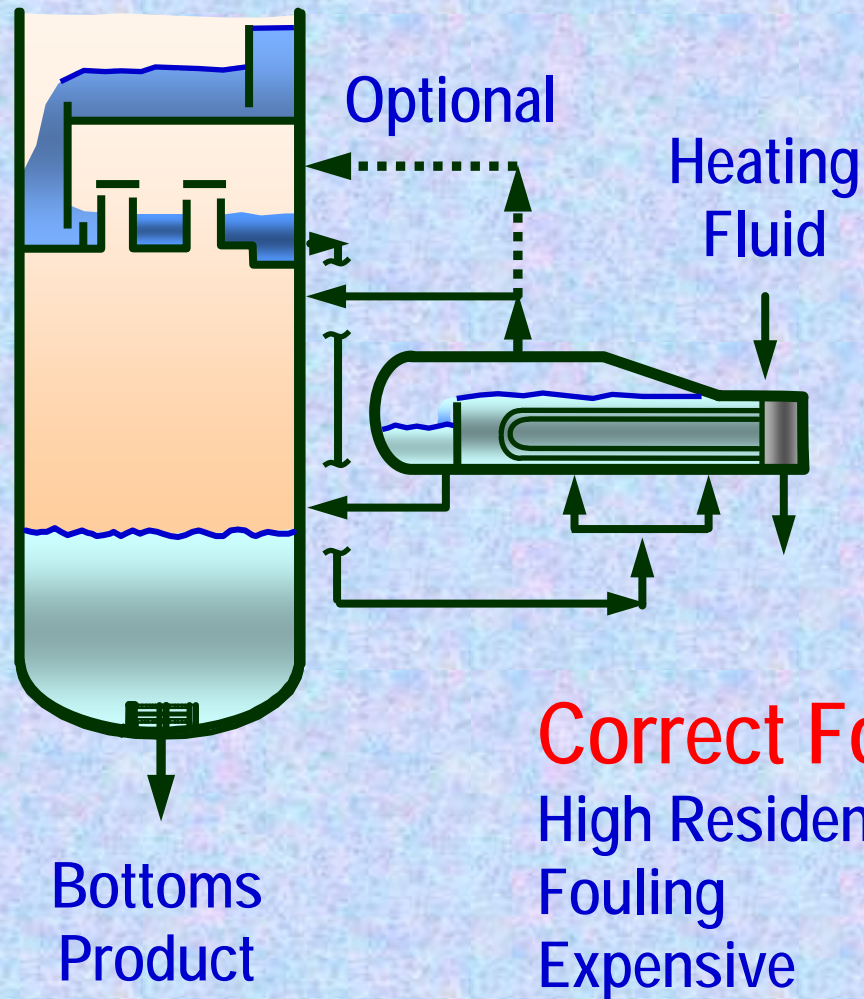
Standard Kettle



Trapout Kettle



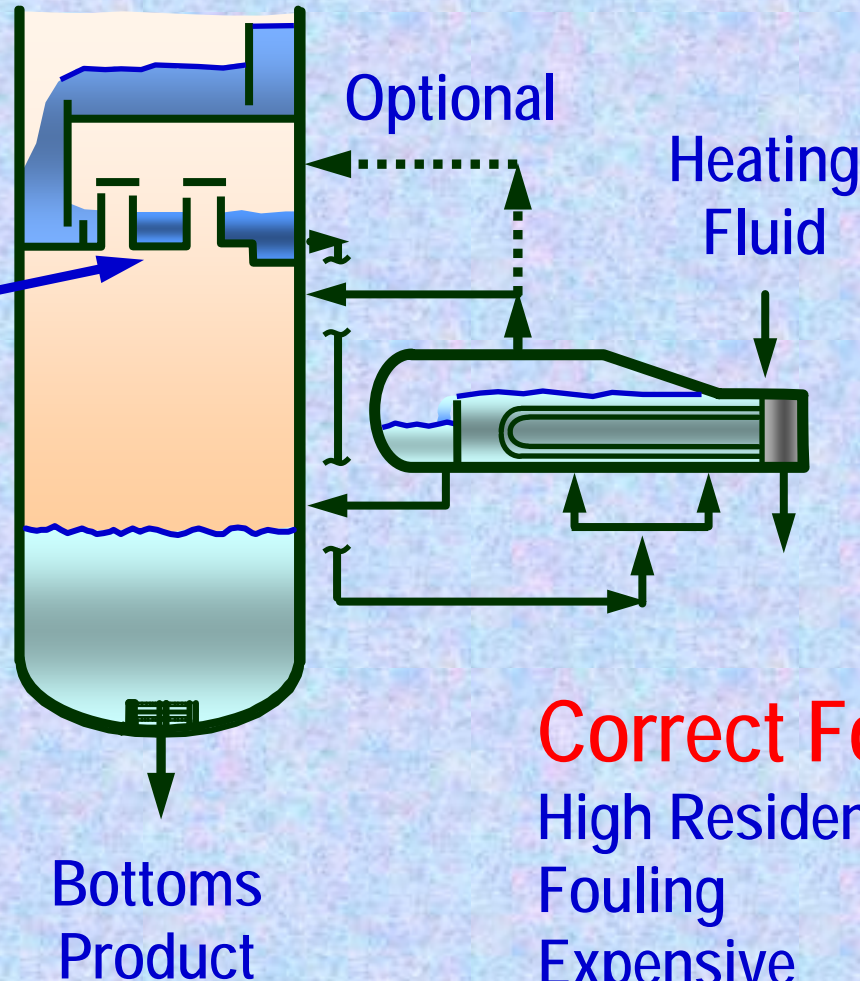
Trapout Kettle



Trapout Kettle

If Trapout NOT
Chimney tray...

Leakage
Reboiler Starved
Undersized Draw



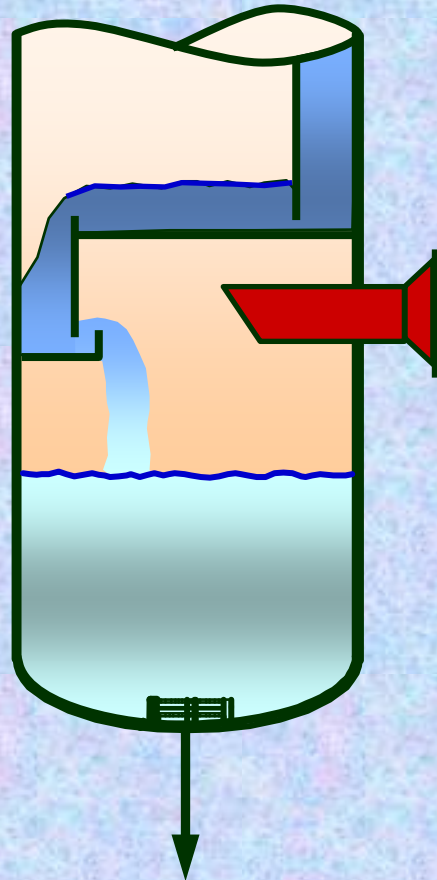
Correct Force Balance

High Residence Time

Fouling

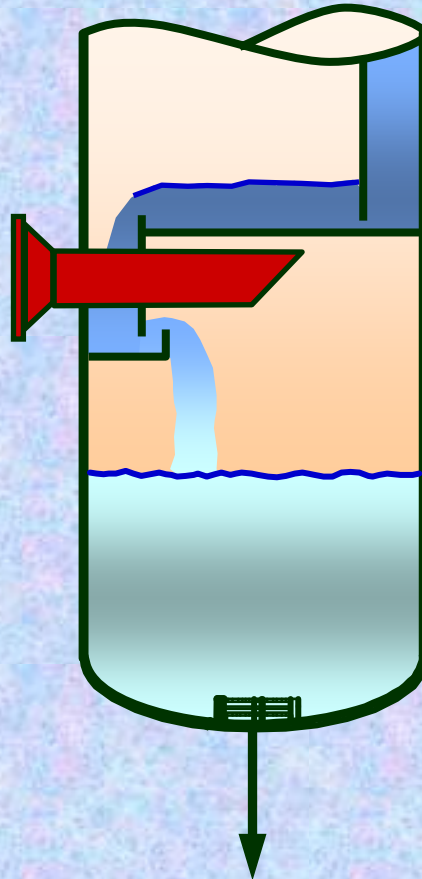
Expensive

Poor Vapor Return Orientation NOT RECOMMENDED



Bottoms
Product

Vapor Return Through Downcomer NOT RECOMMENDED



Bottoms
Product

Questions?

